



# ***CORROSION RESISTANT MATERIALS AND FABRICATION***

**Dennis Lamberth & Chuck Young – Tricor Metals**



# Corrosion Resistant Alloys

- **Stainless Steel** – 304, 304L, 316, 316L
- **Super Austenitic SS** – 904L, Alloy 20, AL6XN, 254SMO
- **Duplex Stainless Steel** - 2205, 2507, 2101
- **Nickel Alloys** – Nickel 200, Monel 400, 625, C276, C2000, 825, B3, Alloy 59
- **Titanium** – Grade 2/2H, 7/7H, 9, 11, 12, 16/16H
- **Zirconium / Tantalum / Niobium**

# Stainless Steel & Duplex SS

## 300" series Stainless Steel

- Iron – Chromium – Nickel alloys
- Intergranular Corrosion (welding & temperature related)
  - Use “L” grade to minimize (lower Carbon)
- Stress Corrosion Cracking possibility
- Used in nitric acid, phosphoric acid (@RT up to 85%), Sulfuric Acid (RT @80%), acetic acid, amines, urea and sulfurous acid

## Duplex Stainless Steel

- PREN # – Improved pitting and crevice-corrosion resistance in Cl<sup>-</sup>
- Yield Strength about 2X SS
- Higher Stress Corrosion Cracking (SCC) resistance than SS
- At 100F use only under 15% Sulfuric or 3% HCl Acids
- Cautions on Welding – heat input, interpass temperature

28

Ni

Nickel

58.6934

2  
8  
16  
2

# Nickel Alloys

- Range of Corrosion Resistance
- Wide variety of Alloys
- Alloys designed for specific corrosives
  - Acidic solutions - Alkali services
  - Chlorine, Marine,
  - Fertilizer manufacturing
  - variety of Chemical Processing

22

 $3d^2 4s^2$ **Ti****Titanium**

47.867

# Titanium Alloys

- Alloys for higher corrosion resistance - Pitting and crevice corrosion - Ti 12, Ti 7, Ti16
- Major CPI Applications
  - Chlorine (WET) & Bromine (WET) & Bleach & Seawater
  - Terephthalic Acid
  - Oxidizing Acids – nitric, chromic, perchloric
  - Low concentrations of Hydrochloric and Sulfuric Acids
  - Alkaline (ammonium hydroxide, sodium hydroxide, etc)
  - Organic Chemicals & Acids (adipic acid, benzene, acetic acid, formic acid)

**40**  
**Zr**  
**Zirconium**  
**91.224**

2  
8  
18  
10  
2

# Zirconium

Zirconium is immune to SCC (Stress Corrosion Cracking) and has very good corrosion resistance in:

- Dry chlorine gas, bromine and iodine gas
- Hydrochloric acid - all concentrations up to boiling
- Nitric acid - all concentrations up to boiling
- Sulfuric acid up to 70% concentration at boiling
- Phosphoric acid up to 60% concentration at boiling
- Urea production
- Most organic acids (e.g. acetic, formic), all concentrations up to boiling temperature



# Alloy Cost Comparison Chart

## Titanium: Affordable and Available



Metal	Density (Lbs/In <sup>3</sup> )	Yield Strength (PSI)	Price/LB	Price/Sq Ft	Price/Sq Ft Normalized
2205	0.29	65,000	\$ 3.04	\$32	\$20
316L	0.29	25,000	\$ 2.80	\$29	\$47
Ti 12	0.163	50,000	\$ 15.07	\$88	\$71
Ti 2	0.163	40,000	\$ 13.34	\$78	\$78
625	0.305	55,000	\$ 14.93	\$164	\$119
C276	0.32	41,000	\$ 13.47	\$155	\$151
CuNi 90-10	0.323	15,000	\$ 7.84	\$91	\$243
Ti 16	0.163	40,000	\$ 60.09	\$353	\$353
Zr	0.234	30,000	\$ 41.73	\$352	\$469
Ti 7	0.163	40,000	\$ 91.25	\$535	\$535

# Project Overview

- **From Project Concept to Final Quality Product**
  - **Design Conditions**
  - **Mechanical Design**
  - **Thermal Design**
  - **Forming**
  - **Welding**
  - **Quality assurance / testing**





# Design Conditions

- Accurately determine design conditions
  - Operating temperature & pressure – upset conditions too
  - Exact PPM of all components of process stream
    - Solids content
    - Other unique concerns (possible deposits)
  - Phase changes / composition changes
  - Process & service flow rates
  - Allowable pressure drops
- Determine proper metallurgy
- Do not “overdesign” in terms of pressure and temperature – Be realistic.



# Other Considerations

- **Physical design decisions**
  - Space limitations / piping hookups in place
  - Materials of Construction (Possible Coupon Testing)
  - Maintain corrosive process to tubeside for cost reduction
  - Maintenance & cleaning considerations
  - U-tube / kettle / reboiler design – TEMA designs
  - Single or double fixed (& welded) tubesheets
  - Maintain corrosive process to tubeside for cost reduction

# Thermal Design

- Performed by a heat transfer expert
- Data sheet filled out by plant engineer
- Materials of construction



# Mechanical Design

- Using ASME guidelines for chosen materials of construction
  - Design allowable stress at operating temperature
  - Maximum operating temperatures
  - Possible upset conditions
- This allows the designer to calculate material thickness
  - Tubes
  - Shell
  - Tubesheets

# Specification Data Sheet

1	Client	COMPANY NAME	Location	CITY or PLANT	Page 1 of 1
2	Process Unit	Line 1	Item No.	HE-4356273-A	Document No.
3	Job No.		Fabricator	TRICOR METALS	
4	Service of Unit	Cooling of process waste water			No. of Units 1
5	Size	TEMA Type (Hor/Vert)	Connected in	Parallel	Series
6	Surface/Unit (Eff.)	ft <sup>2</sup>	Shells/Unit	Surface/Shell (Eff.)	ft <sup>2</sup>
7	PERFORMANCE OF ONE UNIT (Optional)				
8	Fluid Allocation		(Inlet) SHELL SIDE (Outlet)	(Inlet) TUBE SIDE (Outlet)	
9	Fluid Name		COOLING FLUID	PROCESS FLUID	
10	Fluid Quantity, Total	lb/hr	100000	140000	
11	Vapor (MW)	lb/hr			
12	Liquid	lb/hr			
13	Steam	lb/hr			
14	Water	lb/hr			
15	Noncondensable (MW)	lb/hr			
16	Temperature	°F	75	85.0	120.0 108.0
17	Density (Vapor/Liquid)	lb/ft <sup>3</sup>			
18	Viscosity (Vapor/Liquid)	cP			
19	Specific Heat (Vapor/Liquid)	Btu/lb °F			
20	Thermal Conductivity (Vapor/Liquid)	Btu/hr ft °F			
21	Latent Heat	Btu/lb @ °F	@	@	
22	Inlet Pressure	psia/psig	50 psig	75 psig	
23	Velocity	ft/s			
24	Pressure Drop (Allowable/Calculated)	psi	5.	5.	
25	Fouling Resistance	hr ft <sup>2</sup> °F/Btu	0.0010	0.0015	
26	Avg. Film Coefficient	Btu/hr ft <sup>2</sup> °F			
27	Heat Exchanged		Btu/hr MTD (Corrected) (Weighted)		°F
28	Transfer Rate (Required/Fouled/Clean)				Btu/hr ft <sup>2</sup> °F
29	$\rho V^2 - \text{lb/ft-s}^2$ : Inlet Nozzle		Bundle Entrance	Bundle Exit	

# Specification Data Sheet

30	<b>CONSTRUCTION PER SHELL</b>										
31	Tube No.		OD		in	<b>NOZZLES - No. Size &amp; Rating (Optional)</b>					
32	Thickness		in/BWG (Min./Avg.)			<b>SHELL SIDE</b>			<b>TUBE SIDE</b>		
33	Pitch		in	◀	△	◻	◊	Inlet	6"	4"	
34	Length	200	in	Type				Outlet	6"	4"	
35	Tube-Tubesheet Joint							Intermediate			
36	Shell Diameter (ID/OD)							Vent	3/4"	3/4"	
37	Cross Baffle Type							Drain	3/4"	3/4"	
38	Spacing: c/c		in	No. of Crosspasses							
39	% Cut (Dia./Area)										
40	Tube Support					Design Pressure	psig		150	150	
41	Long Baffle Seal Type					Design Temp(Max/MDMT)	°F		400 / 0	400 / 0	
42	By-Pass Seal Type					No. of Passes per Shell					
43	Impingement Protection (Y/N)					Corrosion Allowance	in		1/16"	None	
44	<b>MATERIALS OF CONSTRUCTION (Optional)</b>										
45	Tubes	Titanium all process wetted areas					Gaskets				
46	Shell	316L Stainless Steel					Shell Side				
47	Shell Cover					Tube Side					
48	Channel or Bonnet					Floating Head					
49	Channel Cover					Spare Sets Req'd					
50	Floating Head Cover/Bolts					Test Ring Req'd (Y/N)					
51	Tubesheets					Insulation: Shell					
52	Baffles & Support Plates					Channel Inlet/Exit					
53	Expansion Joint Type			None		Expansion Joint Material					
54	Code Requirements	ASME Sect. VIII					Calc. MAWP (Y/N)	Y		TEMA Class B	
55	REMARKS:	1) Process water contains up to 5% dissolved NaCl									
56											
57											
58											
59	Originator/Check:					Approved:		Issue Date:		Issue No.	A



# Shell & Tube Heat Exchangers

- **Extremely flexible and robust**
- **Wide design capability**
- **Shell and Tube sides can be different materials**
- **Some designs can be dismantled for ease of cleaning**
- **May not be economical for very small applications where custom engineering is required**

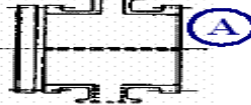
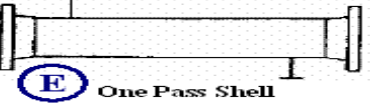

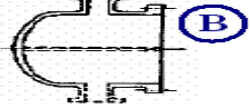
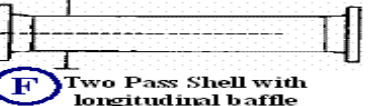
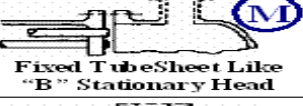
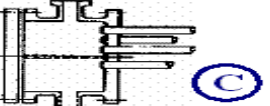
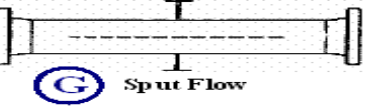
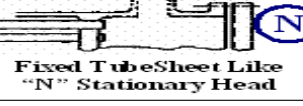
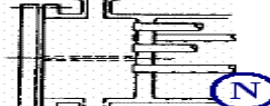
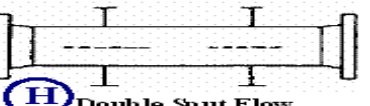

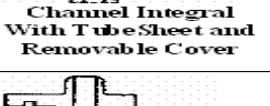
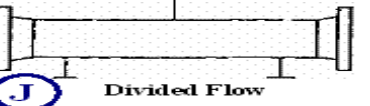

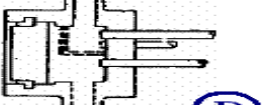
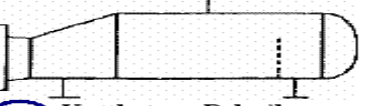
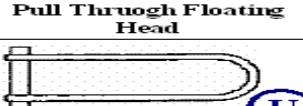

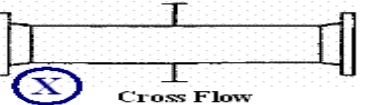
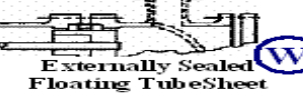


# TEMA Types

- TEMA designations use a three letter code
  - Inlet bonnet
  - Shell type
  - Outlet bonnet
  - Example: BEM



# TEMA Exchanger Designations

Front End Stationary Head types	Shell types	Rear End Head types
 <p><b>A</b> Channel and Removable Cover</p>	 <p><b>E</b> One Pass Shell</p>	 <p><b>L</b> Fixed TubeSheet Like "A" Stationary Head</p>
 <p><b>B</b> Bonnet (Integral Cover)</p>	 <p><b>F</b> Two Pass Shell with longitudinal baffle</p>	 <p><b>M</b> Fixed TubeSheet Like "B" Stationary Head</p>
 <p><b>C</b> Channel Integral With TubeSheet and Removable Cover</p>	 <p><b>G</b> Spurt Flow</p>	 <p><b>N</b> Fixed TubeSheet Like "N" Stationary Head</p>
 <p><b>N</b> Channel Integral With TubeSheet and Removable Cover</p>	 <p><b>H</b> Double Spurt Flow</p>	 <p><b>P</b> Outside Packed Floating Head</p>
 <p><b>D</b> Special High Pressure Closure</p>	 <p><b>J</b> Divided Flow</p>	 <p><b>S</b> Floating Head with Backing Device</p>
 <p><b>D</b> Special High Pressure Closure</p>	 <p><b>K</b> Kettle type Reboiler</p>	 <p><b>U</b> U Tube Bundle</p>
 <p><b>D</b> Special High Pressure Closure</p>	 <p><b>X</b> Cross Flow</p>	 <p><b>W</b> Externally Sealed Floating TubeSheet</p>



# Titanium U-tube Bundle



# Zirconium BKU Heat Exchanger



# Plate & Frame Exchangers

- **High heat transfer surface area**
- **Compact and lower cost than shell and tube**
- **Flexible (easy to add or subtract plates)**
- **Temperature & Pressure Limited**
- **Does not work well with solids**





# Rules of Procurement

- Know what you are buying
- Know your Fabricator
- Don't over design
- Define Quality Requirements
- Define Delivery Requirements
- Lowest price isn't always lowest cost

# Tricor Experience

- Over 28 years in operation
- Management with over 45 years in specialty metals business
- Many welders with over 10 years' experience
- Tricor welder school training – Welding Engineer on staff
- Metallurgist and 2 PE's on staff
- Engineering, Quality Control and Sales with over 35 years' individual experience



# THANK YOU FOR LISTENING

## Tricor Metals

*Cost Effective Corrosion Solutions  
Through Design & Engineering*

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